

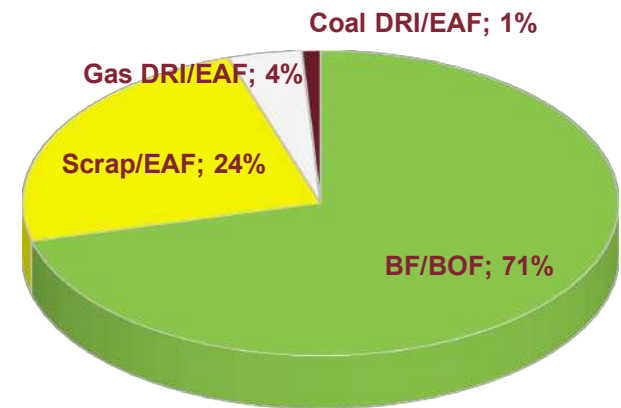
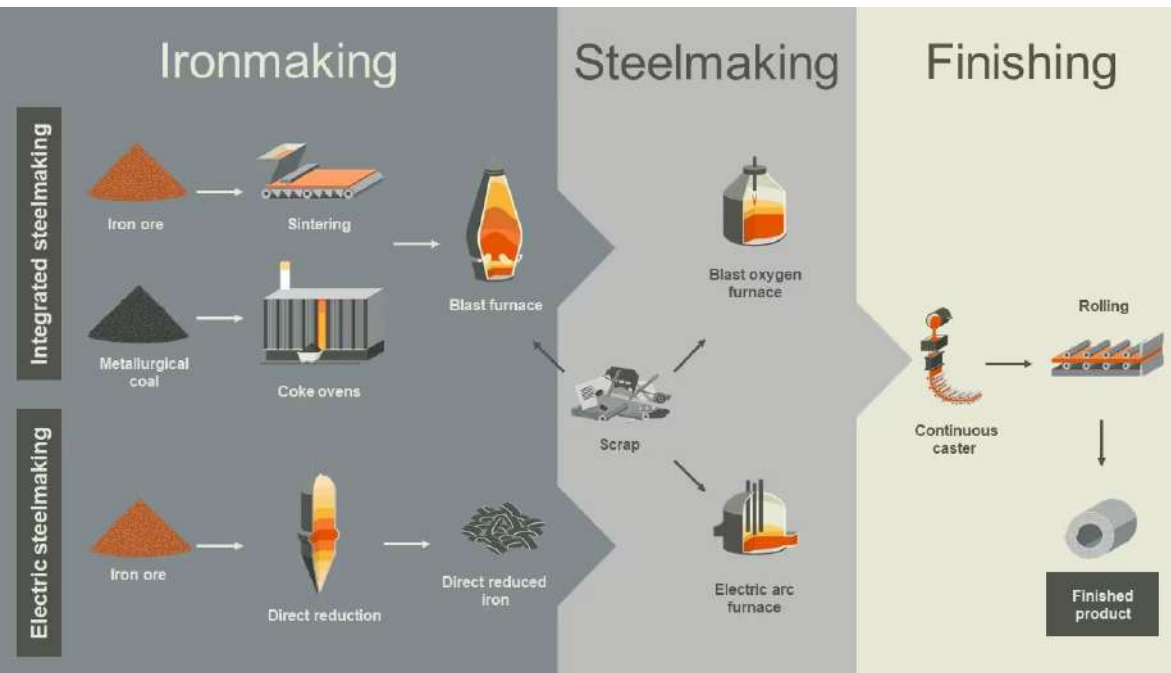
# Decarbonization of steel production: alternative Direct Reduced Iron and CCS

Prof. Giorgio Vilardi  
Ing. Antonio Trinca



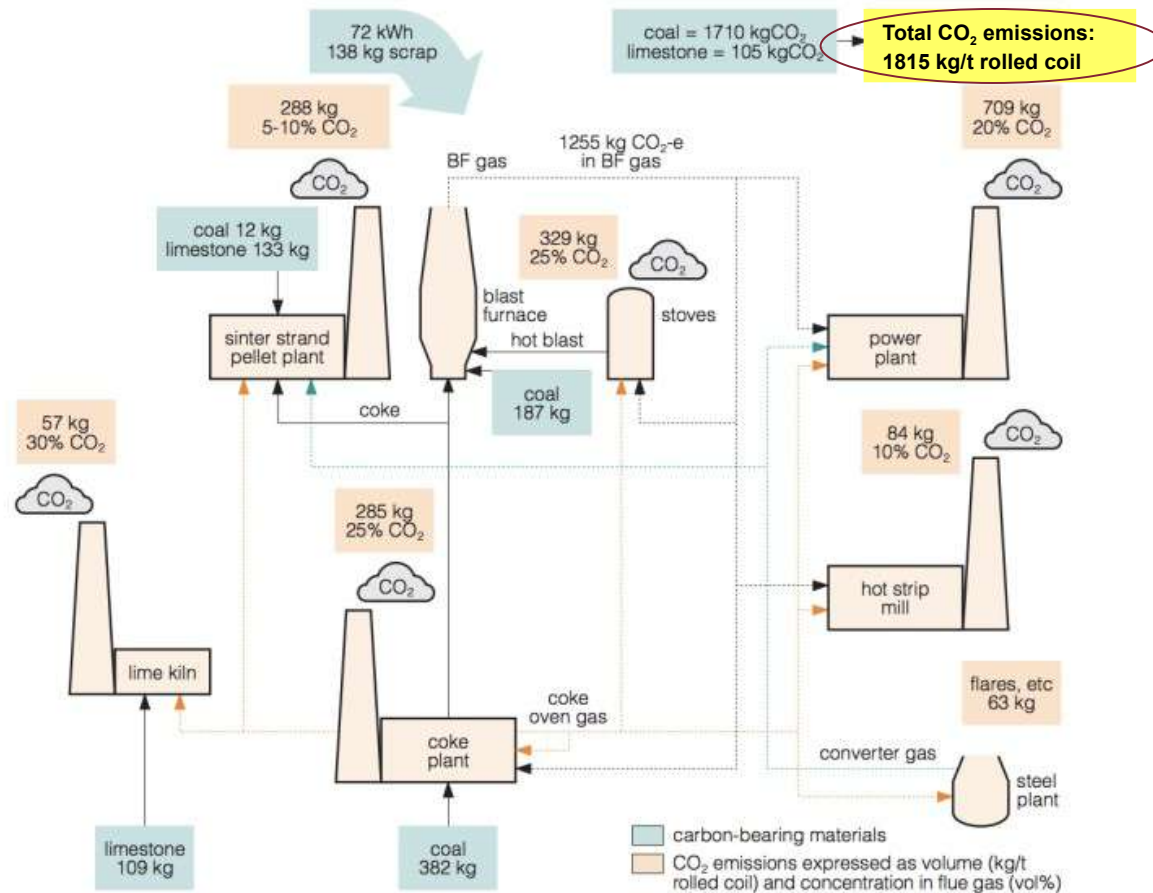
SAPIENZA  
UNIVERSITÀ DI ROMA

# Steel production routes



- Laplace Conseil, “Impacts of energy market developments on the steel industry,” 74th Sess. OECD Steel Comm., no. July, pp. 1–2, 2013

# CO<sub>2</sub> emissions integral cycle BF/BOF



- Bui et al, 'Carbon capture and storage (CCS): the way forward', Energy Environ. Sci., 2018,11, 5, The Royal Society of Chemistry, 10.1039/C7EE02342A.

# CO<sub>2</sub> emissions integral cycle BF/BOF

- Coking making:
  - Coke dry quenching: 27 kgCO<sub>2</sub>/t<sub>coke</sub>
  - COG Recovery: 6-9 GJ/t<sub>coke</sub>
  - Biomass and waste materials: the amount of wood and waste plastics that can be added to the coking coal blend is currently limited to less than 2 wt.% due to detrimental effects on coke quality.
  
- Sintering:
  - Waste Heat recovery and Off-gas recirculation: 60 kgCO<sub>2</sub>/t<sub>sinter</sub>
  - Waste fuels: 19.5 kgCO<sub>2</sub>/t<sub>sinter</sub>
  - Biochar/Charcoal: Up to 20-30% can be used in the sintering bed.

• Cavaliere, P., & Cavaliere, P. (2019). *Clean ironmaking and steelmaking processes: Efficient technologies for greenhouse emissions abatement* (pp. 1-37). Springer International Publishing..

# CO<sub>2</sub> emissions integral cycle BF/BOF

- Blast Furnace

- Injection of:

- COG: saving on coke
    - Oil: 50 kgCO<sub>2</sub>/t<sub>HM</sub>
    - Natural Gas: 55 kgCO<sub>2</sub>/t<sub>HM</sub>

The furnace temperature limits the maximum injection rates. NG has a large effect on the flame temperature cooling with respect to other fuels, so, O<sub>2</sub> enrichment is required.

- H<sub>2</sub>: up to 40%
    - Plastic waste: The substitution of coke is limited to a maximum of around 40% since the injectants are unable to give the physical support for iron ore provided by coke.
    - Biomass

- Cavaliere, P., & Cavaliere, P. (2019). *Clean ironmaking and steelmaking processes: Efficient technologies for greenhouse emissions abatement* (pp. 1-37). Springer International Publishing..

# CO<sub>2</sub> emissions integral cycle BF/BOF

- **Coke** cannot be completely eliminated in the BF operations; its minimum rate is in the order of 200 kg/t<sub>HM</sub>



- Cavaliere, P., & Cavaliere, P. (2019). *Clean ironmaking and steelmaking processes: Efficient technologies for greenhouse emissions abatement* (pp. 1-37). Springer International Publishing..

# Alternative BF/BOF production

- HydroMetallurgy



- Smelting Reduction



- Direct Reduced Iron



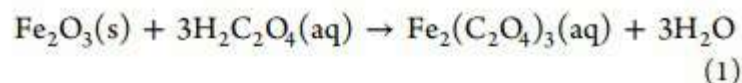
- Hydrogen Smelting Reduction



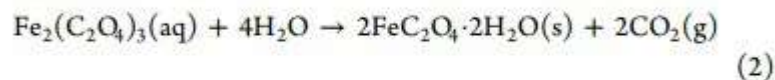
# Alternative BF/BOF production

- HydroMetallurgy  
Acid Leaching

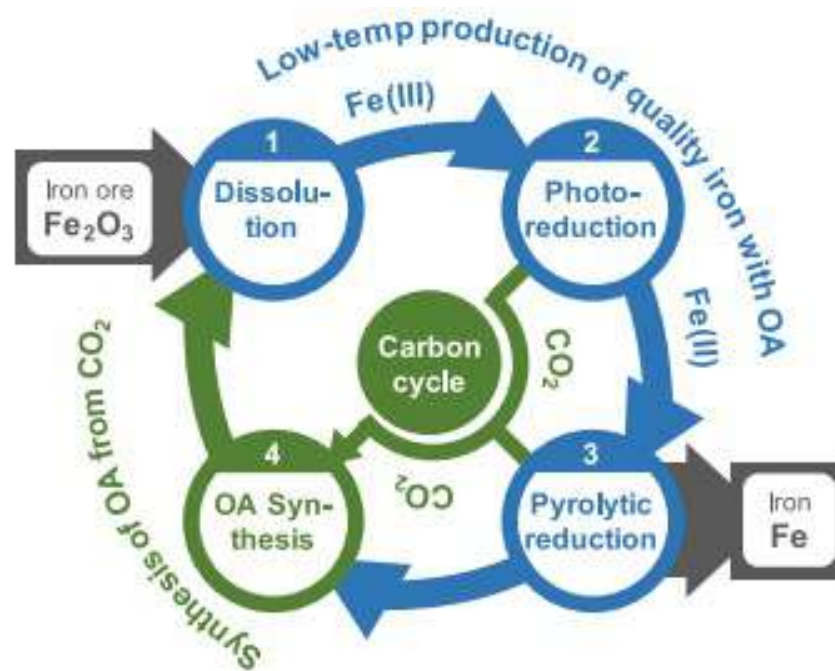
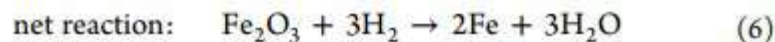
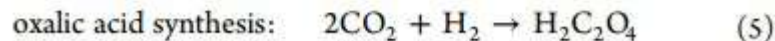
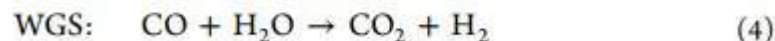
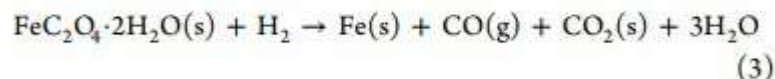
iron dissolution:



photochemical reduction:



pyrolytic reduction:

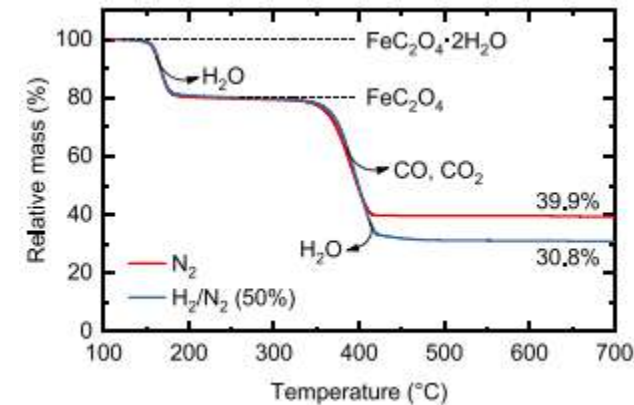
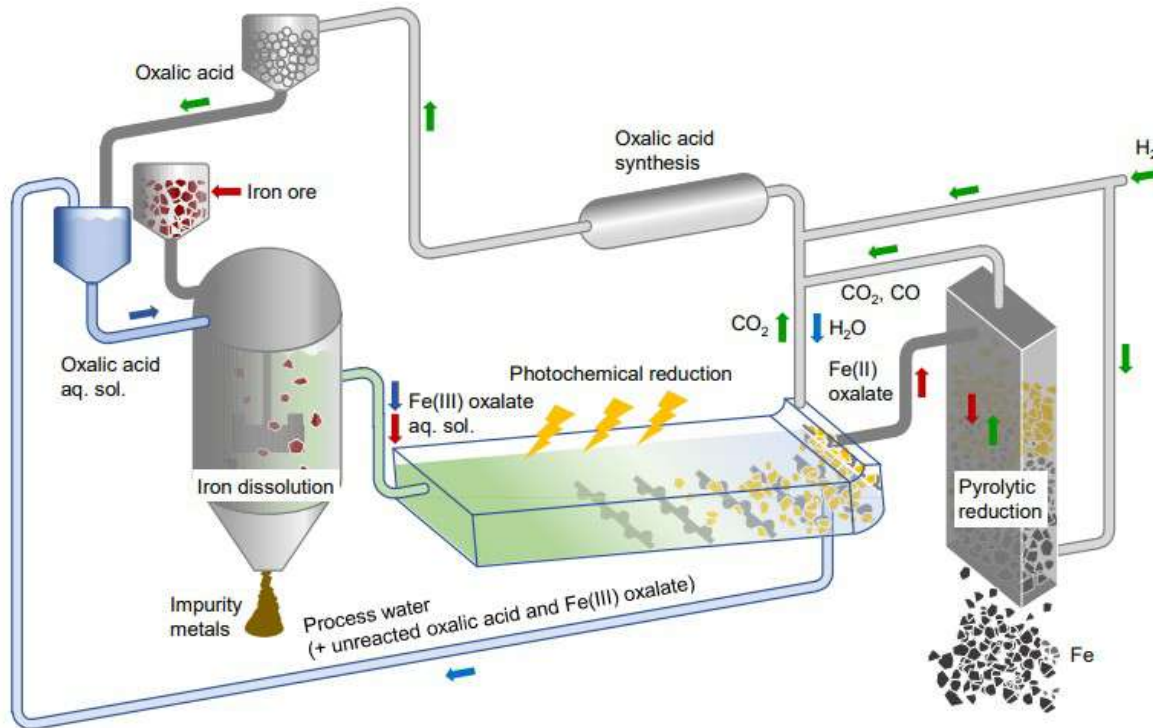


- Santawaja, P., Kudo, S., Mori, A., Tahara, A., Asano, S., & Hayashi, J. I. (2020). Sustainable iron-making using oxalic acid: the concept, a brief review of key reactions, and an experimental demonstration of the iron-making process. *ACS Sustainable Chemistry & Engineering*, 8(35), 13292-13301.



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# Alternative BF/BOF production

- HydroMetallurgy  
Acid Leaching

- Iron purity (on a metal basis): **80.5–99.7 wt %**
  - Feedstocks consisting of **33.9–93.3 wt % iron**
  - Highest temperature: **500 °C**
  - Availability of diverse feedstocks
  - The photochemical reduction needed **6 h** to reach full conversion, with the area fraction of solution surface exposed to light being **17%**
  - Iron productivity **0.5 ton-Fe/day/m<sup>3</sup>** (5–6 h and 0.4–0.5 mol-Fe/L)
- 
- Santawaja, P., Kudo, S., Mori, A., Tahara, A., Asano, S., & Hayashi, J. I. (2020). Sustainable iron-making using oxalic acid: the concept, a brief review of key reactions, and an experimental demonstration of the iron-making process. *ACS Sustainable Chemistry & Engineering*, 8(35), 13292-13301.

# Alternative BF/BOF production

- HydroMetallurgy  
Bio Leaching

- Geobacter metallireducens, Shewanella putrefaciens and L. ferriphilum reduce  $\text{Fe}^{+3}$  to  $\text{Fe}^{+2}$  under anaerobic conditions
- No need for coke
- Energy consumption reduction by 2,080 MJ/t of iron compared to the blast furnace
- The  $\text{CO}_2$  directly emitted by the process entirely from biomass
- Efficiency of **93.85%** iron was achieved with L. ferriphilum, at 313 K at the end of **20 days**
- TC, E. (2005). Direct Biohydrometallurgical Extraction of Iron from Ore. Final Technical Report (No. INIS-US--0697). Michigan Technological University (United States). Funding organisation: US Department of Energy (United States)

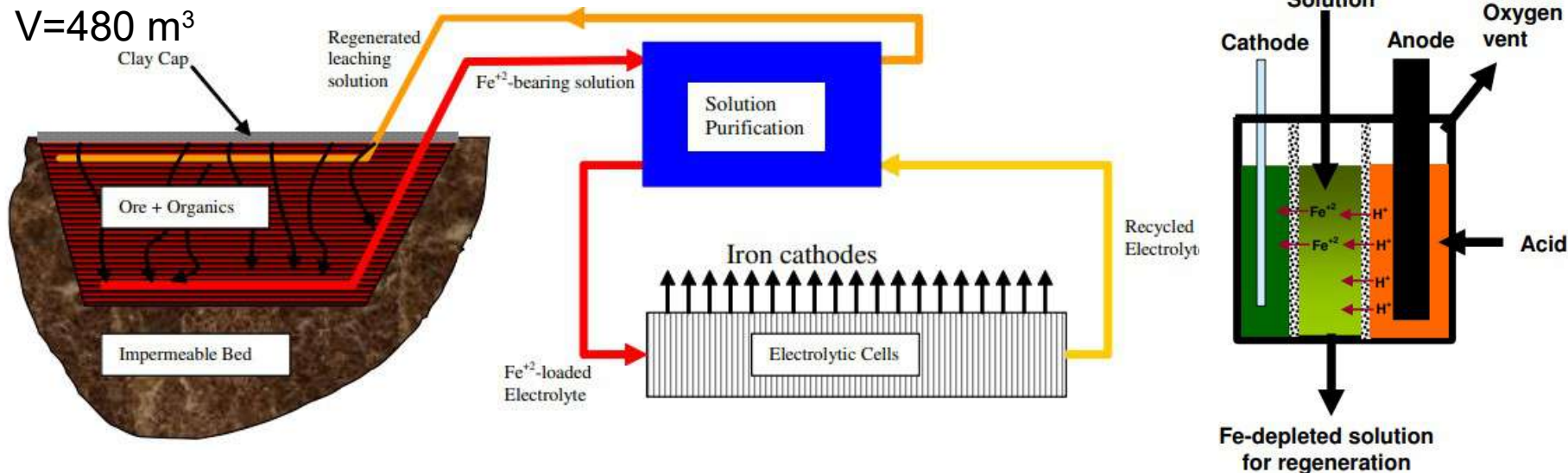
# Alternative BF/BOF production

- HydroMetallurgy  
Bio Leaching

$t_{res} = 20 \text{ d}$

$Qv = 1 \text{ m}^3/\text{h}$

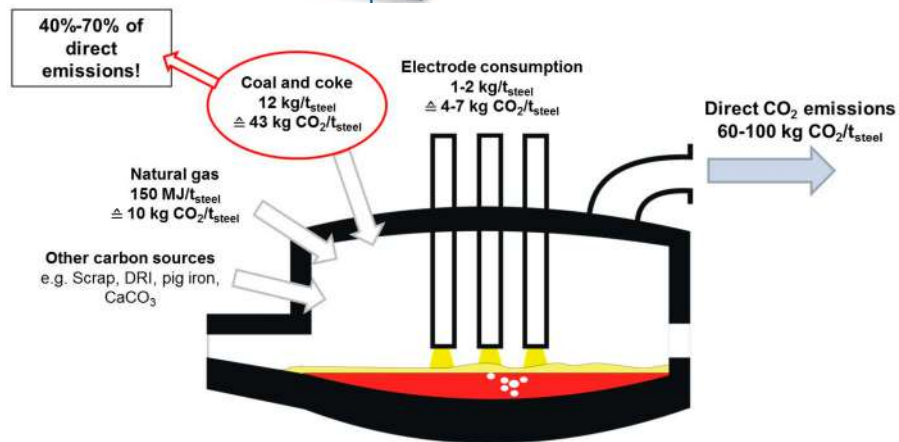
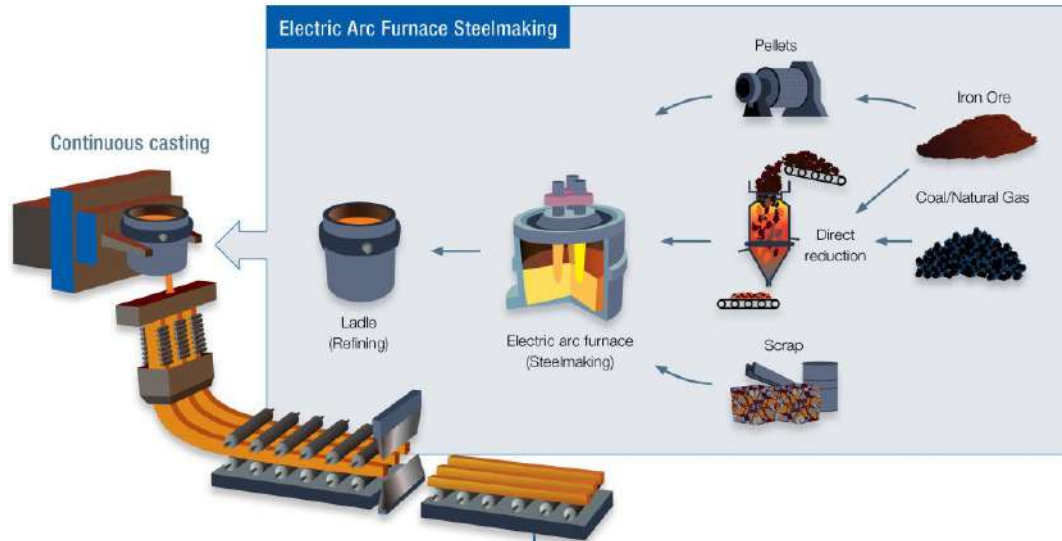
$V = 480 \text{ m}^3$



- TC, E. (2005). Direct Biohydrometallurgical Extraction of Iron from Ore. Final Technical Report (No. INIS-US--0697). Michigan Technological University (United States). Funding organisation: US Department of Energy (United States)
- Prabhu, S. V., Ramesh, G., Adugna, A. T., Beyan, S. M., & Assefa, K. G. (2019). Kinetics of iron bioleaching using isolated *Leptospirillum ferriphilum*: effect of temperature. International Journal of Innovative Technology and Exploring Engineering, 8, 76-81.

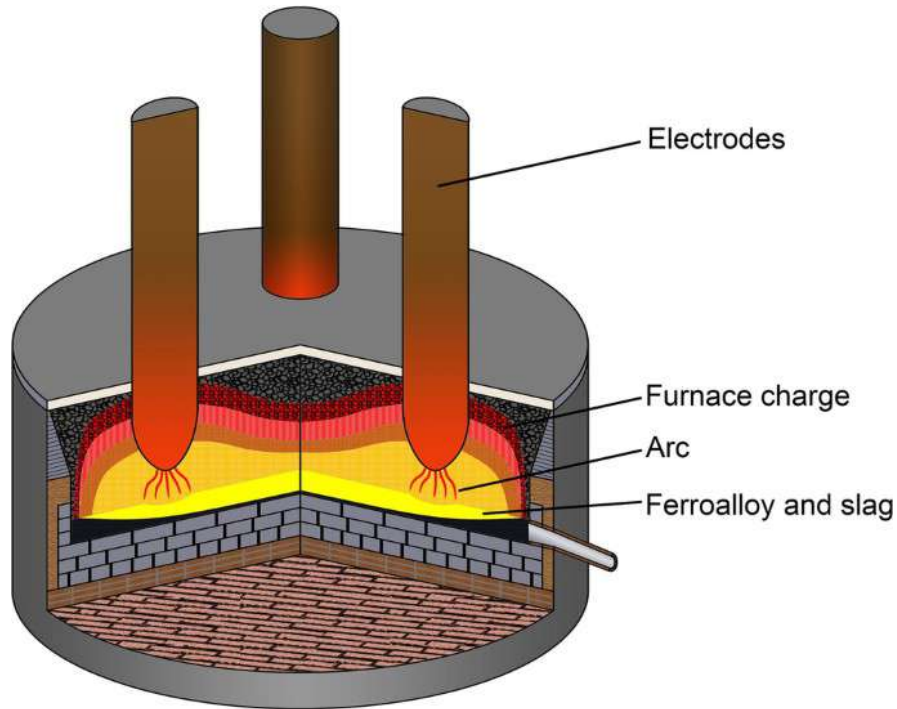
# Alternative BF/BOF production

- Smelting Reduction  
Electric Arc Furnace



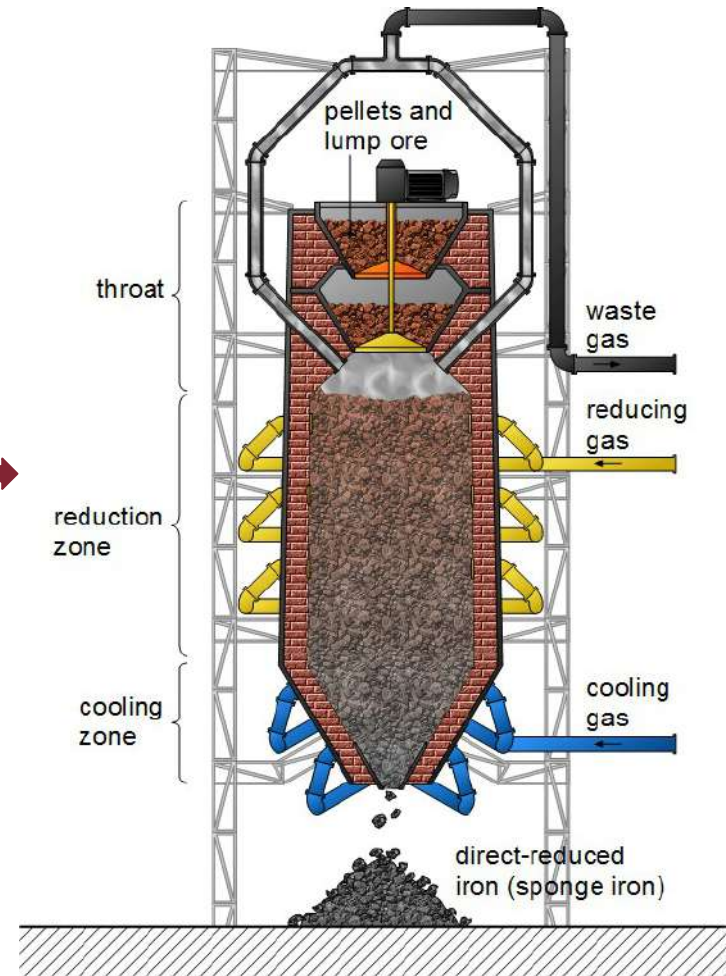
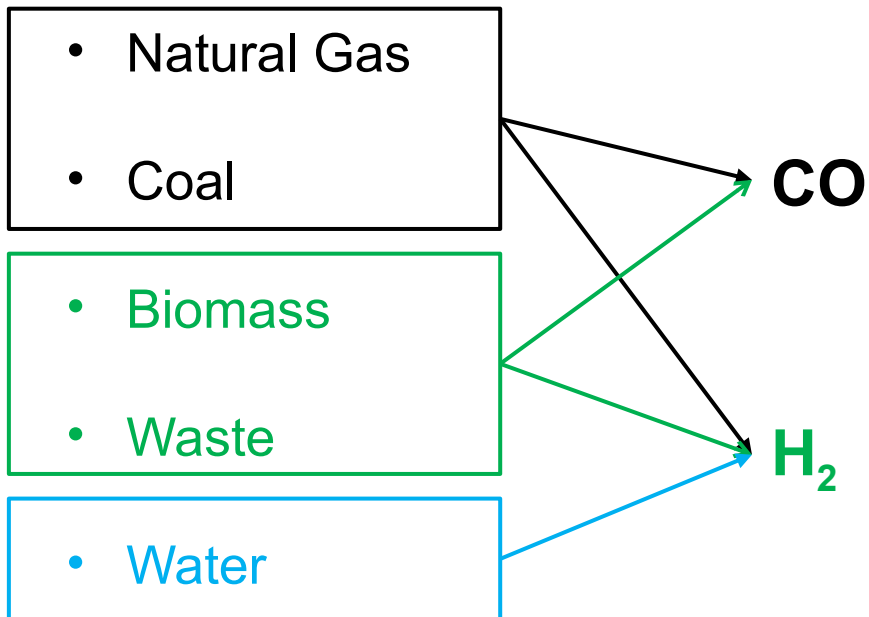
# Alternative BF/BOF production

- Smelting Reduction  
Submerged Arc Furnace



# Alternative BF/BOF production

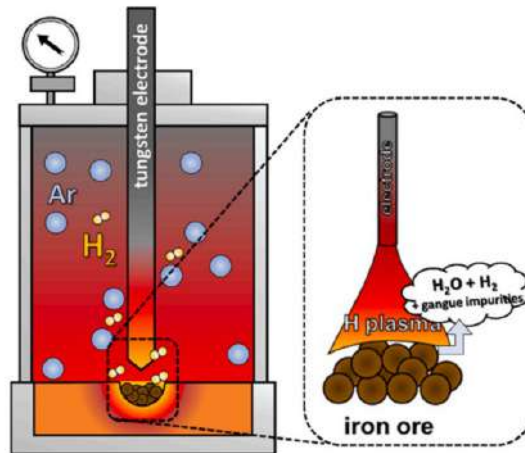
- Direct Reduced Iron



# Alternative BF/BOF production

## • Hydrogen Smelting Reduction

- Simultaneous reduction and melting
- Reduction potential of atomic and ionic  $H_2$  present in  $H_2$  plasma is, respectively, **3** and **15** times higher than molecular  $H_2$
- **2000-2600 °C** at the interface between the plasma arc and the oxide melt
- Close to **100% reduction**

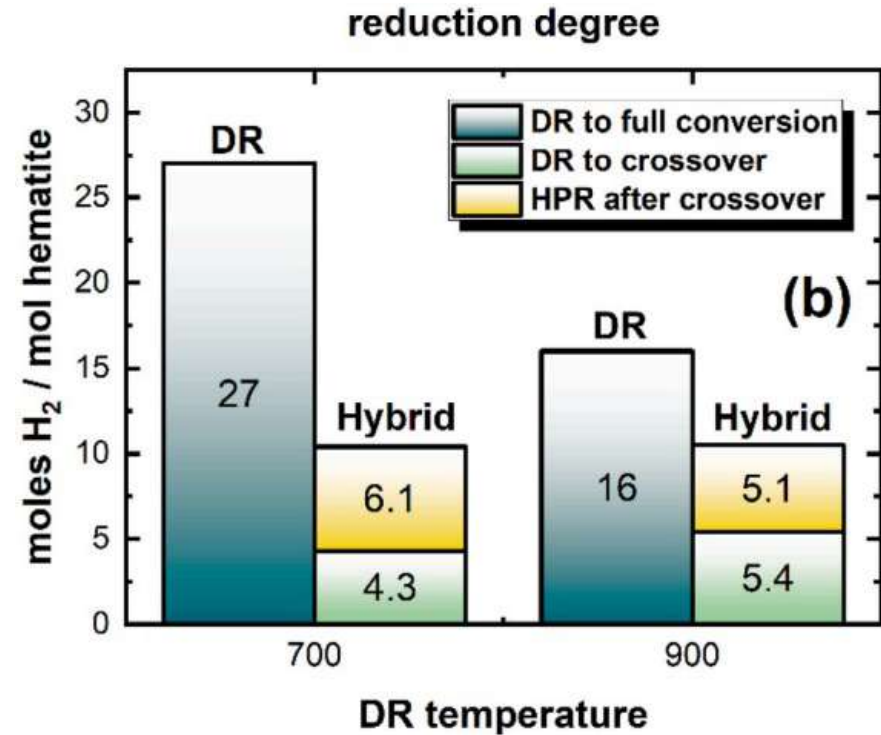
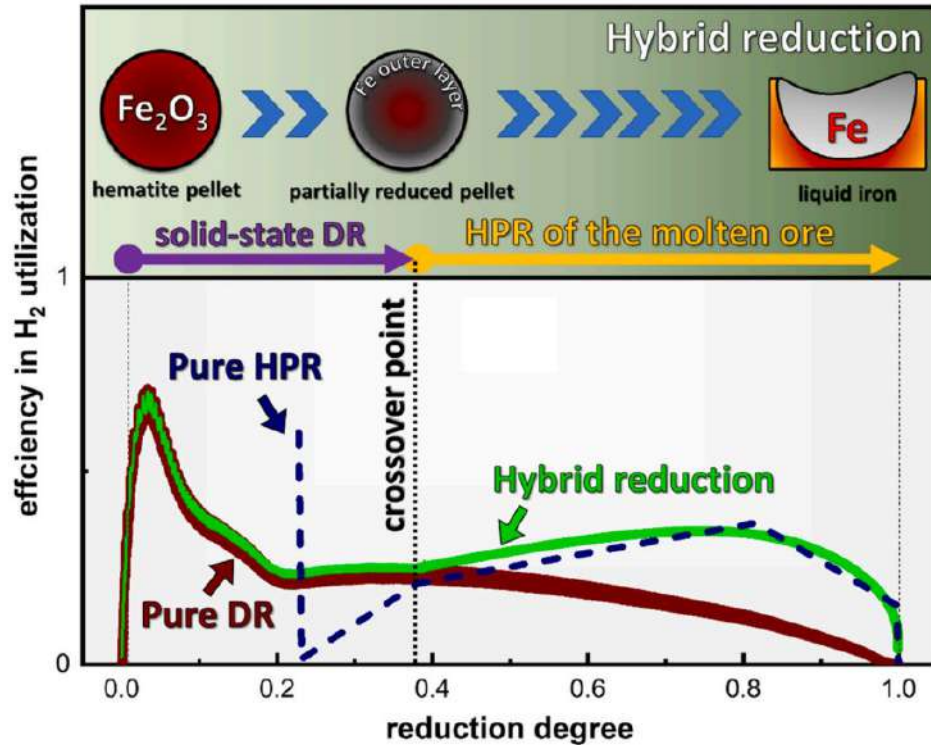


- Souza Filho, I. R., Springer, H., Ma, Y., Mahajan, A., da Silva, C. C., Kulse, M., & Raabe, D. (2022). Green steel at its crossroads: Hybrid hydrogen-based reduction of iron ores. *Journal of Cleaner Production*, 340, 130805.
- Behera, P.R., Bhoi, B., Paramguru, R.K. et al. Hydrogen Plasma Smelting Reduction of Fe<sub>2</sub>O<sub>3</sub>. *Metall Mater Trans B* 50, 262–270 (2019). <https://doi.org/10.1007/s11663-018-1464-8>



# Alternative BF/BOF production

- Hydrogen Smelting Reduction



- Souza Filho, I. R., Springer, H., Ma, Y., Mahajan, A., da Silva, C. C., Kulse, M., & Raabe, D. (2022). Green steel at its crossroads: Hybrid hydrogen-based reduction of iron ores. *Journal of Cleaner Production*, 340, 130805.

# Carbon Capture in the Steel Industry



# Carbon Capture in the Steel Industry

- CO<sub>2</sub> removal consists of:
- PSA, VPSA
  - VSPA/PSA + Cryogenic Separation
  - Chemical Absorption

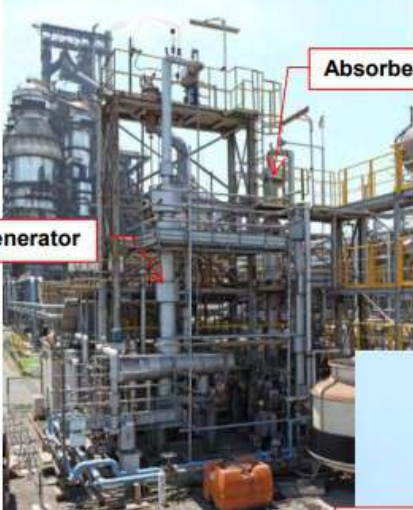
	PSA	VPSA	PSA+cryogenic separation+ compression	VPSA+compression + cryogenic separation	Amines+ compression
<i>CO<sub>2</sub>-rich gas captured</i>					
CO <sub>2</sub> (% vol)	79.7	87.2	100	96.3	100
Suitable for transport and storage?	no	no	yes	yes	yes
<i>CCS Process</i>					
Electricity consumption (kWh/tCO <sub>2</sub> )	100	105	310	292	170
Capture Process (kWh/tCO <sub>2</sub> )	100	105	195	160	55
Compression to 11 MPa for storage (kWh/tCO <sub>2</sub> )	-	-	115	132	115
Steam consumption (GJ/tCO <sub>2</sub> )	0	0	0	0	3.2
<b>Total energy consumption (GJ/tCO<sub>2</sub>)</b>	<b>0.36</b>	<b>0.38</b>	<b>1.12</b>	<b>1.05</b>	<b>3.81</b>

# Carbon Capture in the Steel Industry

## COURSE 50 Programme

### **CAT-1 & CAT-10**

at Nippon Steel Kimitsu Works



#### **CAT-1**

1 t/d CO<sub>2</sub> for solvent testing

Regenerator

Absorber

Off Gas

CO<sub>2</sub>

Regenerator

Reboiler

#### **CAT-30**

30 t/d CO<sub>2</sub> for process improvement evaluation



### **ASCOA**

at JFE Steel Fukuyama Works

#### **ASCOA-3\*** (JFE Steel Fukuyama Area)

\*Advanced Separation System by Carbon Oxides Adsorption

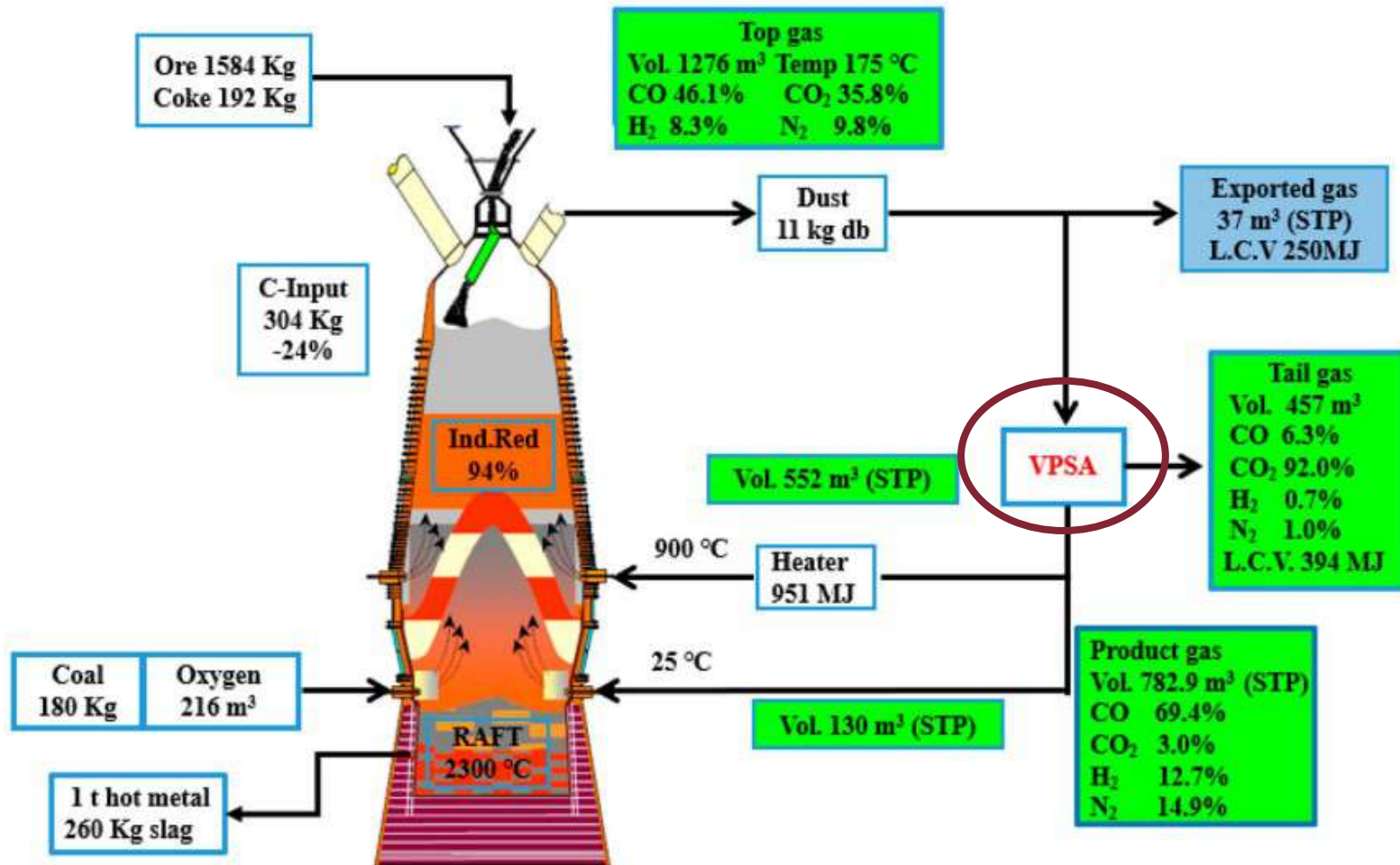
Capacity : 3tons-CO<sub>2</sub>/day  
Plant Area : 21m x 25m



Start : March 2011

# Carbon Capture in the Steel Industry

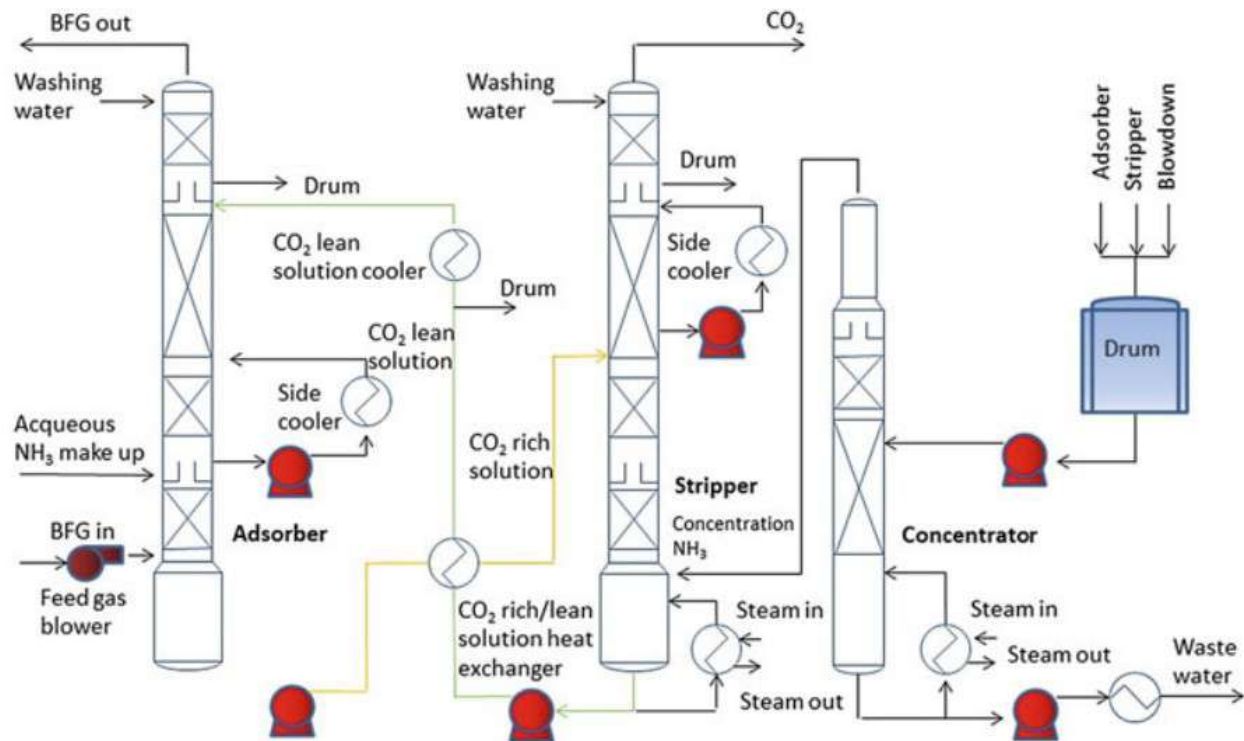
## Ultra-Low CO<sub>2</sub> Steelmaking (ULCOS) Programme



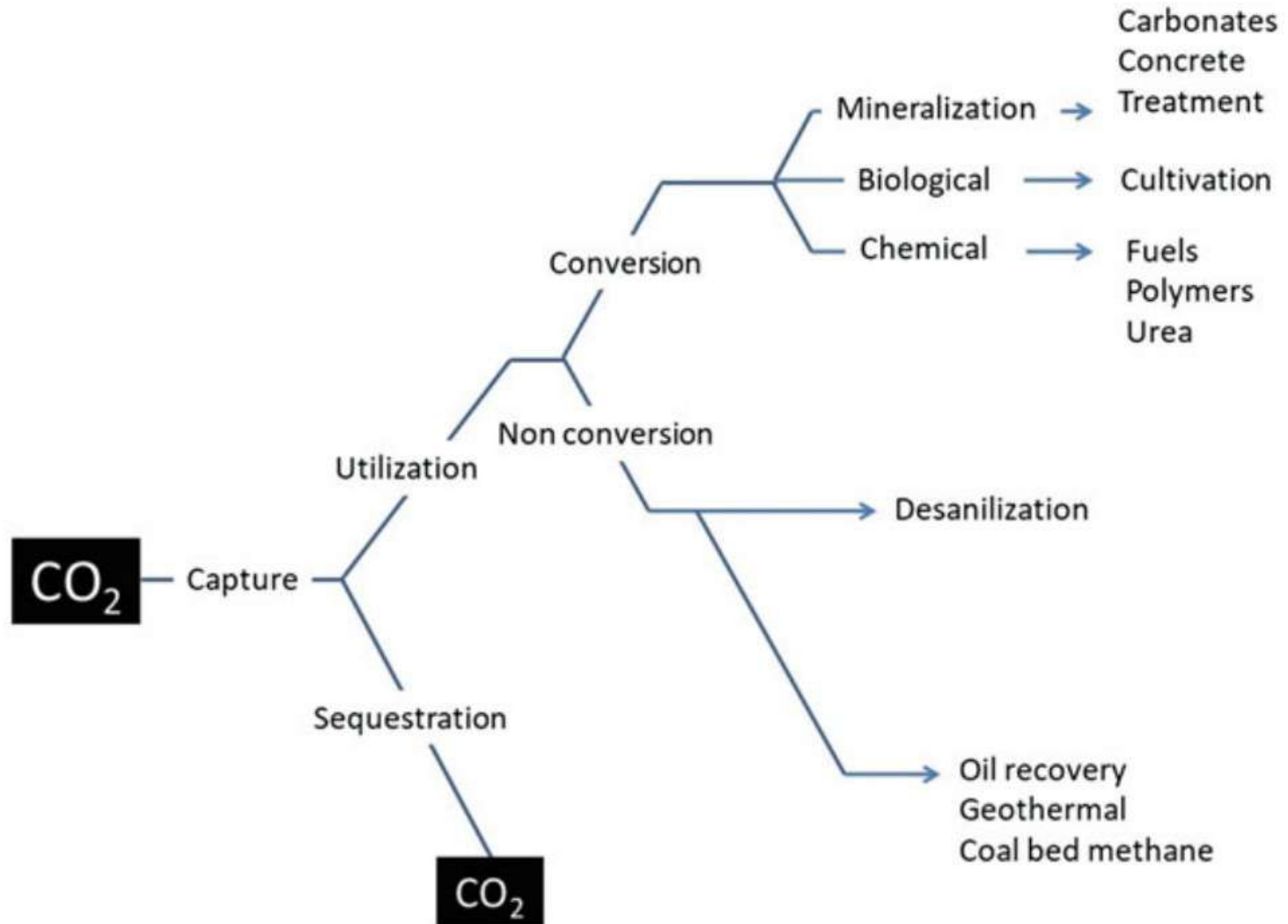
# Carbon Capture in the Steel Industry

## POSCO Programme

<b>Feed Gas</b>	<b>BFG (CO<sub>2</sub>-22%)</b>
<b>Flow Rate</b>	1000 Nm <sub>3</sub> /h
<b>Absorbent Solvent</b>	10% NH <sub>3</sub>
<b>CO<sub>2</sub> Absorption</b>	10 tCO <sub>2</sub> /d
<b>Purity</b>	> 99.5%
<b>Recovery</b>	> 90%



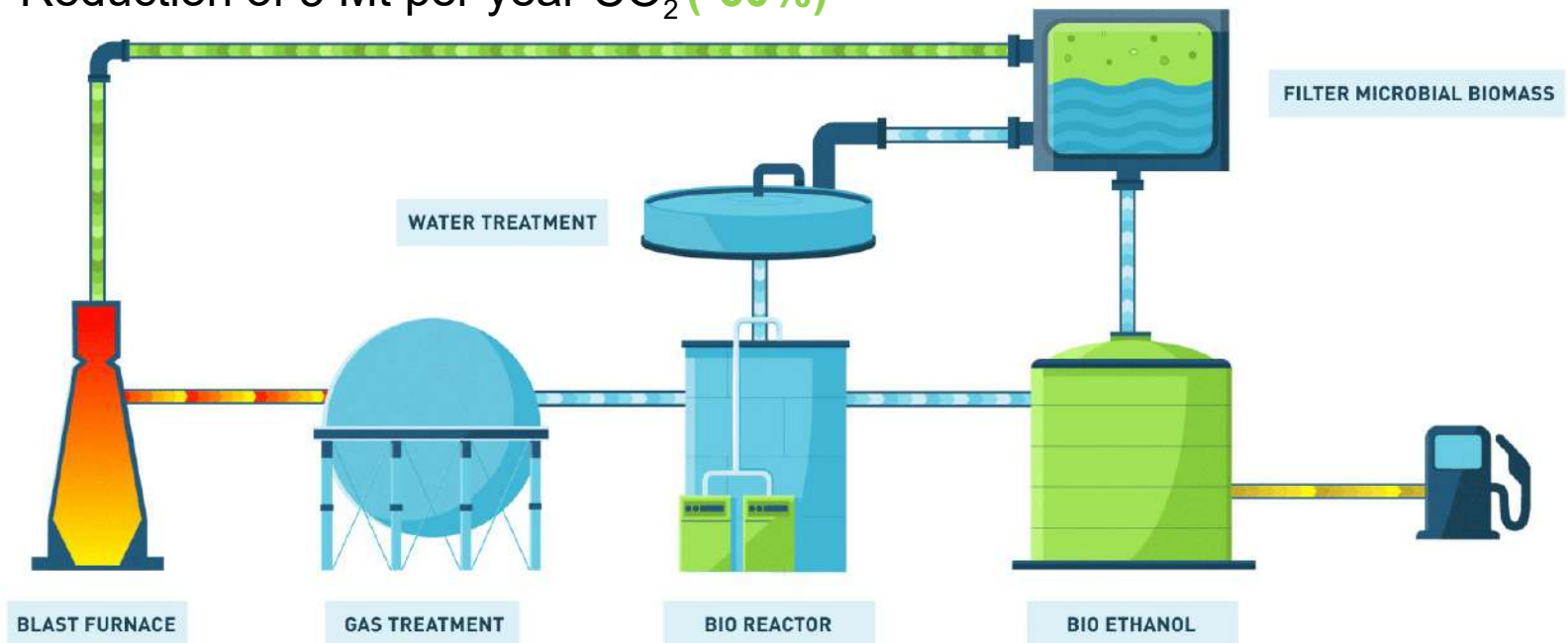
# Carbon Capture in the Steel Industry



# Carbon Capture in the Steel Industry

## Steelanol Programme

- 165 M€ investment
- 80 million liters of bioethanol annually
- Every 2.3 tons of CO<sub>2</sub> captured equals one ton of ethanol
- Reduction of 5 Mt per year CO<sub>2</sub> (-60%)

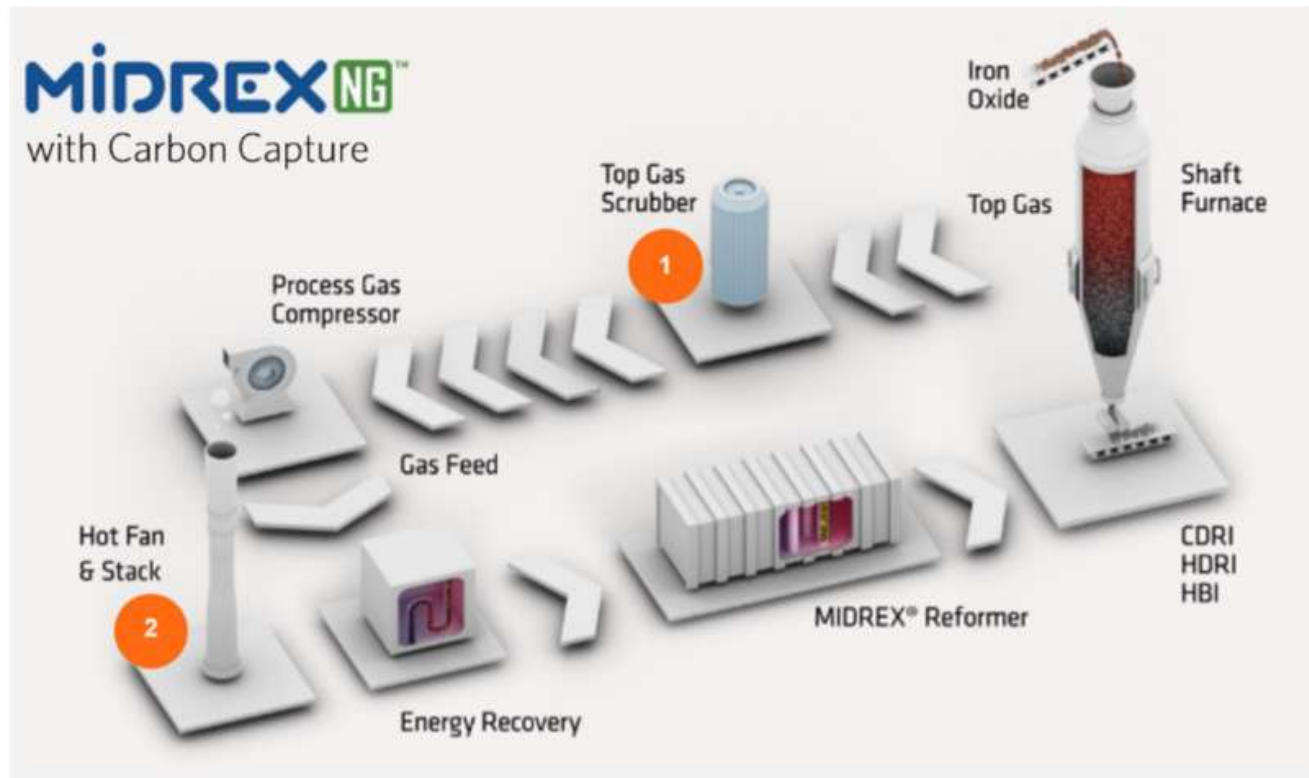




# Carbon Capture in DRI

## MIDREX Process

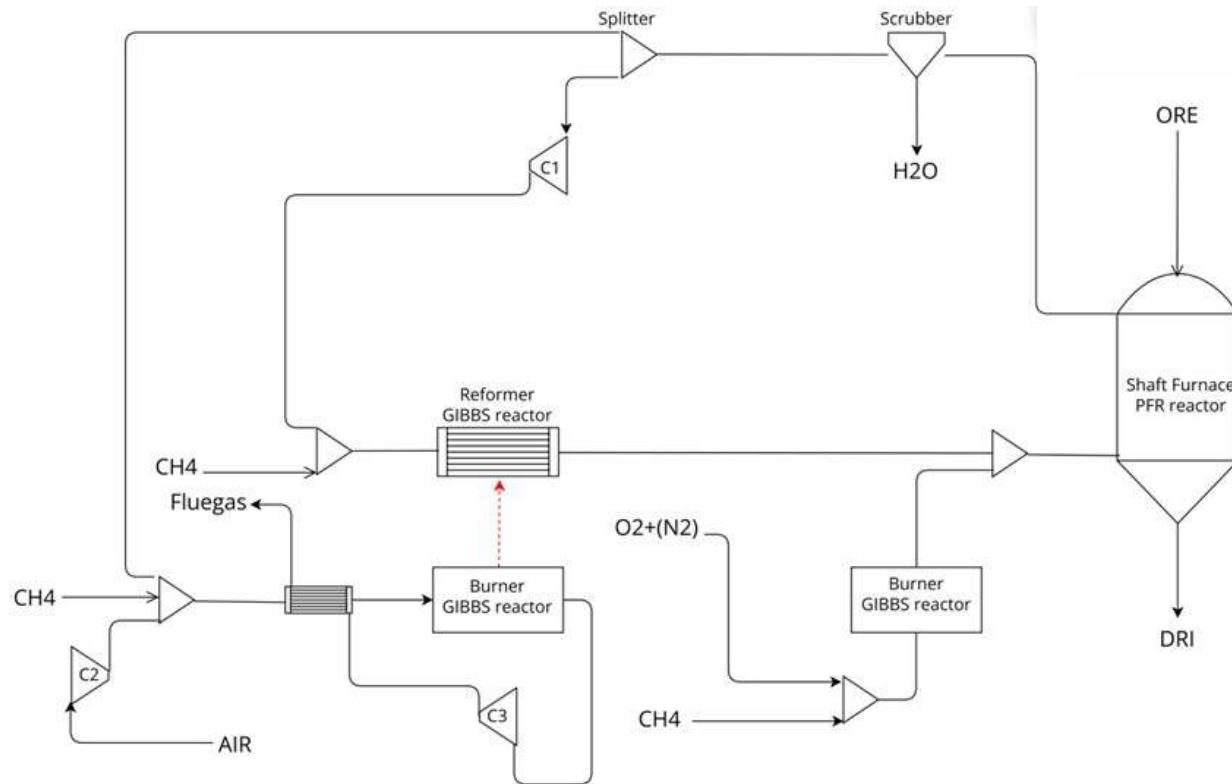
- No standalone Midrex Plant that removes CO<sub>2</sub> from the DRI shaft reactor's off-gas.



# Carbon Capture in DRI

## MIDREX Process

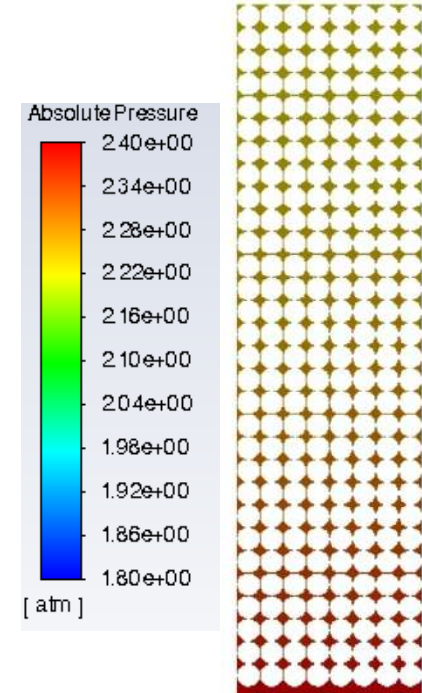
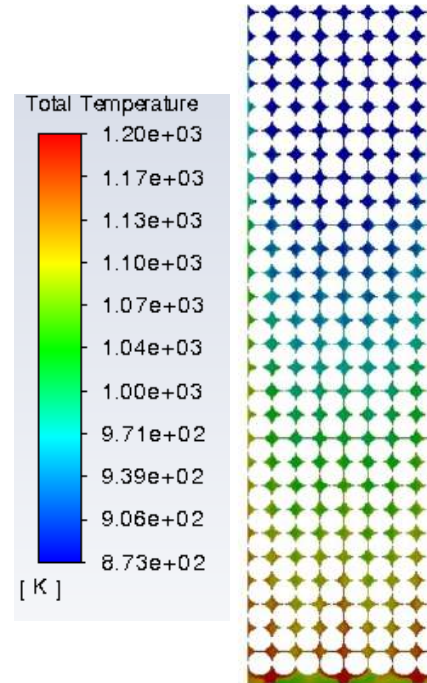
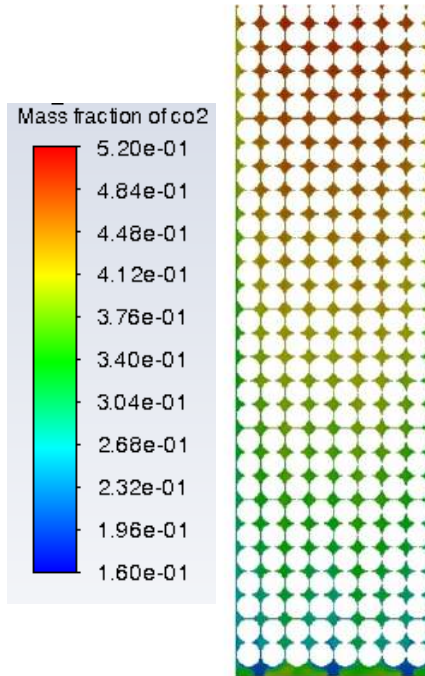
Gilmore Steel Corporation (U.S.A.)



# Carbon Capture in DRI

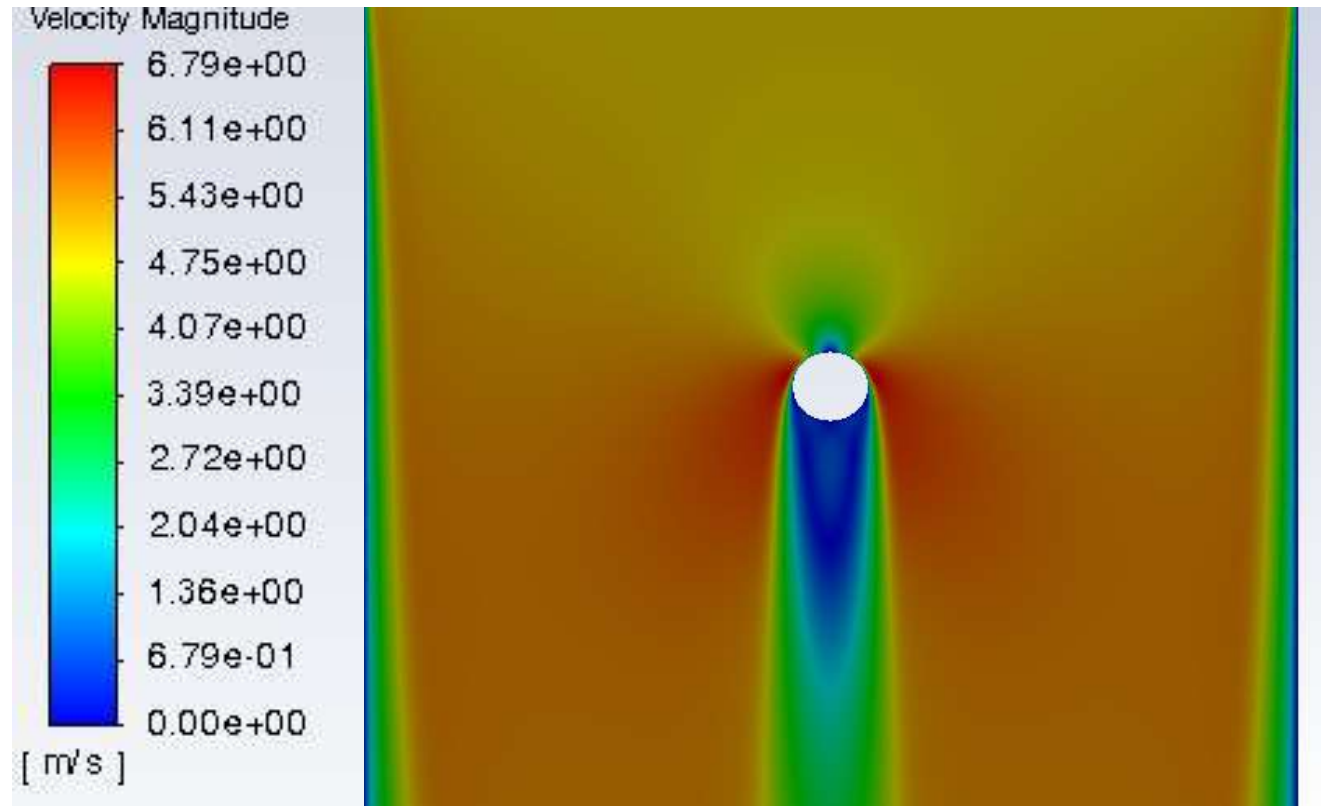
## MIDREX Process

### Gilmore Reduction Shaft



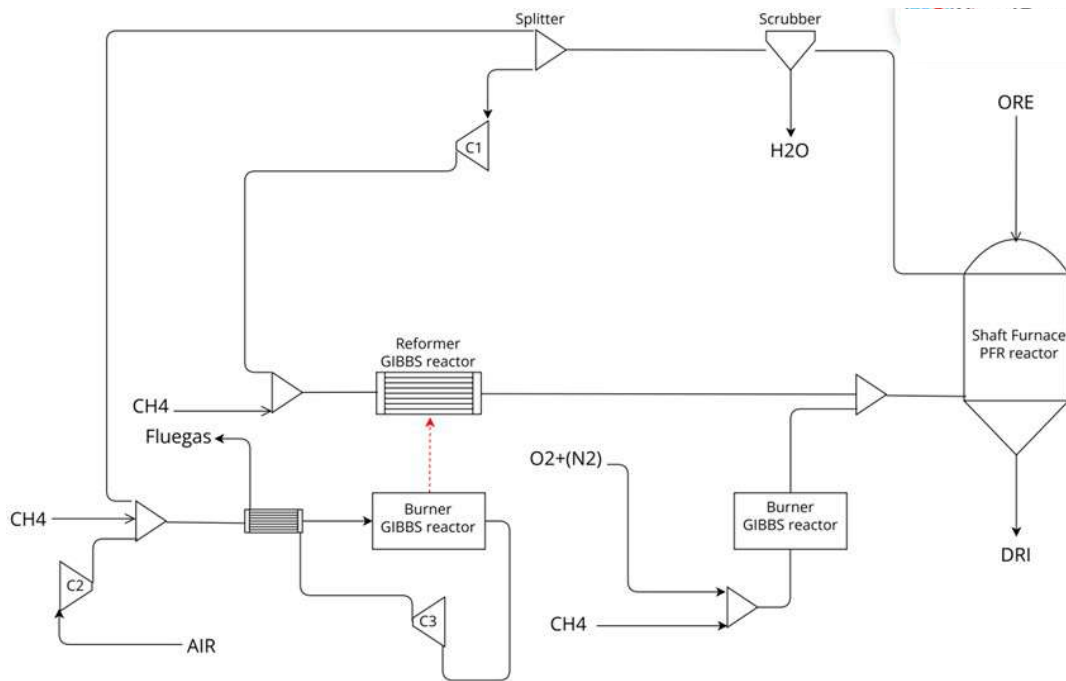
# Carbon Capture in tDRI

## MIDREX Process



# Carbon Capture in the Steel Industry

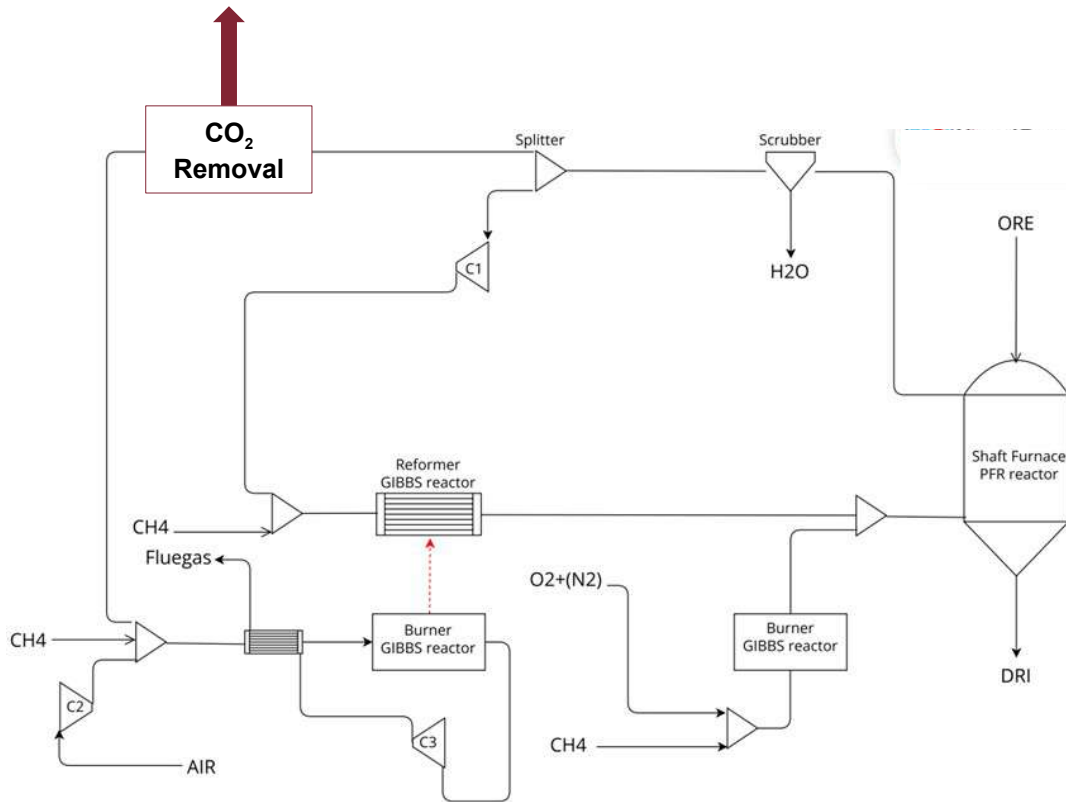
## MIDREX Process



<u>Inlet reducing gas</u>		
Flow rate	Nm <sup>3</sup> /h	53,862.31
Temperature	°C	930
Pressure	bar	2.4
Composition		
H <sub>2</sub>	%	48.19
CO	%	25.40
H <sub>2</sub> O	%	13.85
CO <sub>2</sub>	%	5.43
N <sub>2</sub> (+CH <sub>4</sub> )	%	7.13
<u>Outlet gas</u>		
Flowrate	Nm <sup>3</sup> /h	53,799.74
Temperature	°C	660
Composition		
H <sub>2</sub>	%	37.04
CO	%	12.80
CO <sub>2</sub>	%	<b>17.98</b>
H <sub>2</sub> O	%	25.13
N <sub>2</sub> (+CH <sub>4</sub> )	%	7.01

# Carbon Capture in the Steel Industry

## MIDREX Process

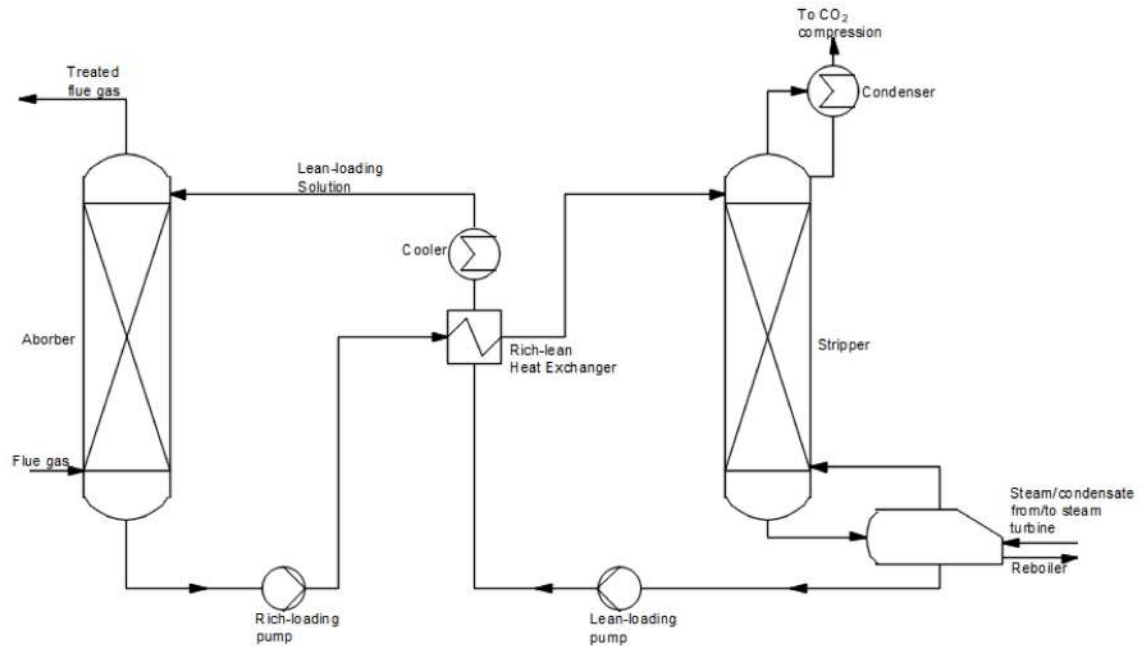


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CO <sub>2</sub>	%	<b>17.98</b>
H <sub>2</sub> O	%	25.13
N <sub>2</sub> (+CH <sub>4</sub> )	%	7.01

# Carbon Capture in the Steel Industry

## MIDREX Process

<b>Feed Gas</b>	<b>CO<sub>2</sub>-30% (dry)</b>
<b>Flow Rate</b>	13017.80 kg/h
<b>Absorbent Solvent</b>	30% MEA
<b>Purity</b>	96.6%
<b>Recovery</b>	95%



### Specific Emission (t<sub>CO2</sub>/t<sub>STEEL</sub>)

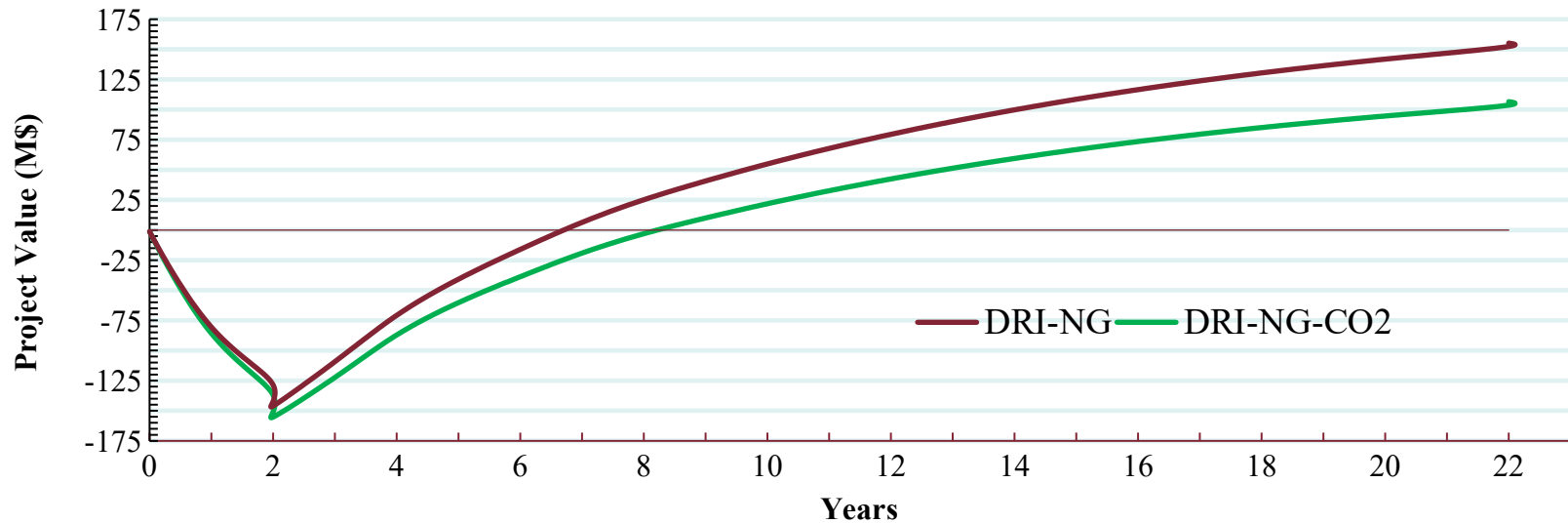
	<b>DRI-NG</b>	<b>DRI-NG+Carbon Capture</b>
Direct	0.46	0.19
Equivalent	0.14	0.15
<b>Total</b>	<b>0.60</b>	<b>0.34</b>

# Carbon Capture in the Steel Industry

## MIDREX Process

Production cost (\$/t):

- Chemical Absorption: **+ 8.7%**
- Chemical Absorption + Storage/Transport: **+10.5%**



	Unit	DRI-NG	DRI-NG CO <sub>2</sub>
NPV	M\$	155.11	106.55
ROI	%	23.62	19.27
PBT	y	3.90	4.98



# Decarbonization of steel production: alternative Direct Reduced Iron and CCS

**Prof. Giorgio Vilardi**

**Ing. Antonio Trinca**

Research group: <https://giorgiovilardi.wixsite.com/dracons>

